INDIAN COALS FOR SPONGE IRON PROCESS

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Abstract

IN CONTRAST to conventional two stage process of steel making via blast furnace, direct steel making with pre-reduced iron ores or agglomerates have attra cted attention in recent times. This is particularly so for developing countries where there is availability of other raw materials for iron making but there is dearth of or limited resources of coking coal and abundant supply of other type of non coking coals. In terms of energy equivalent, availability of solid fuel is many hundred times more than that of natural gas. Extensive attempts have therefore been made to utilise non coking coals to produce iron by non conventional methods such as direct reduction processes. The solid iron produced by reduction technique known as 'sponge' can then be transformed into steel by melting.

An attempt has been made in the paper to indicate the available resources of Indian coals, their nature and property which may be considered suitable for the production of sponge i ron either as such or after beneficiation. Indications have also been given for the possibility of utilising char from the fluid bed carbonisation of non coking coal where such material can be obtained from an integrated formed coke plant.

Introduction

The Conventional two-stages process of steel making via blast furnace has been in vogue over a century. In recent times, for reason of economy and productivity, large sized blast furnaces have been installed, which calls for stringent specifications for the raw materials, particularly the coke. For coke with superior physical properties, good quality coking coals have to be used. The shortage of such coking coals the world over, therefore, becomes the chief bottleneck in the expansion of iron and steel industry. Attempts are being made to conserve this valuable raw material in the following ways:

- i) By reducing intake of good quality coking blend by incorporating medium and pre-determined blends, followed by improved techniques of coal preparation and carbonisation.
- ii) By injecting auxiliary fuels like coal, oil, coal-oil slurry, gas etc. at the tuyeres of the blast furnaces with improvement in operation such as by raising the blast

temperature, oxygen content of the blast, humidification of the blast and by high top pressure of the blast furnace.

- iii) By utilising alternate fuels prepared from non coking coals in the form of 'formed coke.'
- iv) Lastly, attempts are being made to bypass the blast furnace technique altogether by adopting direct reduction technique for the production of iron-(sponge iron) followed by melting in electric furnace.

The idea to produce iron without the use of the blast furnace has been a favoured objective of the metallurgist during the past several decades. Numerous processes 1,7 have been suggested and reviewed which aim at producing iron in the soild form and not in the liquid state as in the blast furnace practice.

In a recent analysis Miller (3) has forecast that while steel production in the world would reach a total of 735 million tons in 1975 and 915 million tons by 1980, the production and consumption of pre-reduced ore would equal to 11 million and 62 million tons respectively in those years.

Direct Reduction Processes

Directly reduced iron ore is neither iron nor ore as one normally understand either of the components. It is nothing more than the reduction of oxygen in the ore below the melting and fusion point of the ores, pellets or agglomerates. For a given mass of ore, the total iron weight remains unchanged even though metallic iron is increased by a reduction in the oxygen combined with it. With oxygen removal a honeycombed microstructure remains which is called 'sponge iron.' The term is used inter-changeably with pre-reduced agglomerates and directly reduced iron ores.

It is possible to use reducing agents (solid or gaseous reductants) other than coke, which are also cheaper in most of the cases. In this context, it will be worthwhile to consider the quantum of "available" reductants in the world⁵ against the "total" reserve in India (expressed in terms of 101⁵ K. cals).

World	India
47000	461.7
11000	5.6
730	1.7
	0.8
	World 47000 11000 730

From the above it is seen that the reserves of coal are about several hundred times larger than that of natural gas. Due to this and also in view of the ability of the processes utilising solid reductants to handle a variety of raw materials, many plants^{4,5} are in operation in various countries as may be seen in Table 1.

The limited resources of coking coal in India are well known. The imbalance between the availability1,8,9 of quality iron ore and good quality coking coal has been emphasised many a time. In Fig. 1 is given the distribution of the iron ore and coal resources of India. In the years to come it is also likely that pig iron plants may be installed in locations away from the coking coal areas. In this context, two points of great significance emerge. They are (i) the production and utilisation of formed coke10 from non coking coals as an alternate fuel for blast furnaces and (ii) consideration of the increasing application of non conventional techniques for the reduction of iron oxide, by passing the standard blast furnace route.

In the Krupp-Renn process,4 reduction is

carried out in an inclined rotary kiln, fired by pulverised coal, and coke is used as the solid reductant. Though this process is adopted in several countries, the consumption of fuel is high. It is stated that about 150-250 kg of coke per ton of 'luppen' produced is required for which about 350 kg of coal dust is also fired in the kiln.

The SL/RN process⁴, for which also an inclined rotary kiln is employed for reduction, has been adopted in many countries. Almost any solid carbonaceous material may be used as heating and reducing agent. Low rank high volatile coals having low strength and with fusion temperature of ash above 1150° C may be used with advantage for the reduction. It has, also been mentioned that heat requirement varies from 2.37×10^{6} to 3.5×10^{6} K. cal per ton of sponge iron.

Considering this, it may be pointed out that the large reserves of non coking coal (about 80% of the total reserve) available in the country and even char made of low temperature by fluid bed carbonisation may be used as reductants for the production of sponge iron. Ghosh and Lahiri2 have also suggested suitability of the solid reduction technique in India. Recently Miller and Koring7 have reiterated that direct reduction technique can make a good impact for the ambitious iron and steel plans India is drawing up. In the direct reduction process, for the manufacture of spcnge iron, high volatile, non coking coals with relatively high ash fusion point particularly the initial deformation (I.D.) temperature (> 1150°C) appear to be most desirable. In addition the coals should be low to medium in ash. with relatively low sulphur (< 1.0%) and phosphorus (< 0.1%)

Resources of Indian Coals Available for Direct Reduction

A detailed study of the available information on the nature and composition of coals occurring in India shows that unlike coking coals, non caking coals are well distributed all over the Lower Gondwana coal basins of the peninsular India (Figure 1). In Table II are compiled the nature, composition and resoure potentialities^{11,12} of the solid minerals fuels ranging from lignite to bituminous coals which are likely to conform to the specifications of solid fuels suitable for the manufacture of sponge iron by the direct reduction process.

Non coking coals with ash ranging normally between 11% and 24% (on air dried basis), and volatile matter between 25% and 35% (on air dried basis) have been largely selected. Moreover, due



consideration is necessary for lower contents of total sulphur, phosphorus and relatively higher initial deformation temperature of the ash in mildly reducing atmosphere (> 150 °C). The areas of occurrence of coal seams containing coals of the specifications are restricted to central and eastern sectors of the Raniganj Measures coals of Raniganj coalfield in the East, Sone Mahanadi valley coalfields of Madhya Pradesh and Orissa, and the Pench Valley coalfields in the West. The coals also are found to underline in the South in the Kamptee, Wardha valley coalfields of Maharashtra and the Godavari valley coalfields of Andhra Pradesh. In further South, there occurs the lignite deposit of Neyveli in Tamil Nadu. The proved reserves of such coals from seams under exploitation total to over 5600 million tonnes excluding 600 million tonnes of proved reserves of Neyveli lignite. This estimate excludes all coking, medium coking, semi to weekly coking coals of Jharia. Raniganj, East and West Bokaro, Ramgarh, Jhilmili and Kanhan valley coalfields and the semi to weaklycoking, high sulphur tertiary coals of Assam.

i) Raniganj coalfield

The Central and Eastern part of Raniganj coalfield accounts for a total reserve of non coking coals of over 2300 million tonnes available from 7 to 8 working coal horizons. Thickness of the seams generally varies between 1.2 and 9 metres. The coals are high in volatile (31 to 35% air dried) with ash mostly below 20%. The I.D. temperatures of the coal ash are often somewhat lower, ranging between 1100° —1210°C.

ii) North and South Karanpura Coalfields

The total reserves of the working coal horizons of these two coalfields amount over 1000 million tonnes. In north Karanpura coalfield, δ to 9 coal horizons (viz-Bachra, Karkata, Bisrampur, Bukbuka, Dakra, etc.) generally ranging in thickness between 1.5 and 6 metres are being exploited. The ash in these coals vary widely-even from the same coal horizon, which at times exceeds 28%. The I.D. temperature of the coal ash is, however, high (above 1250°C). In South Karanpura coalfield 10 to 12 upper coal horizons (Argada 'A' and above) are being exploited whose thickness ranges generally between 2 and 7 metres. Argada seam is a thick coal horizon (11 to 54 metres). The ash of the coals from the seams also varies widely and often tends to go quite high. The initial deformation temperature of the coal ash is at times lower which ranges between 1100° to 1280°C.

iii) Sohagpur Coalfield

In Sohagpur coalfield of Madhya Pradesh, Burhar, Kotma and Jhagrakhand are the three potential areas which account for a total reserve of over 260 million tonnes of coals. These are available from 1 to 3 working coal horizons whose thickness range between 2 to 8 metres. The coals there from are fair to medium in quality, the percentage ash being mostly below 20%. The coals are high in volatiles (24 to 31% air dried) and low in sulphur (below 0.8%) and phosphorus (below 0.01%). The initial deformation temperature of the coal ash is b tween 112.) C to 1350°C.

Of the three, Burhar area appears to be promising as the coals can be had from a single source (i.e. Dhanpuri Seam) of a composite unit. In the single unit there is a reserve of over 100 million tonnes of coal. The volatiles and fusion temperatuhe (I.D.) of the coals are also on the higher side.

iv) Chirimiri Coalfield

This coalifield accounts for a total reserve of over 430 million tonnes of non coking coals from 1 to 3 working coal horizons (viz. Korankoh/ Bijora/Gorghela/Main, 3A, Sonawani etc.) whose thickness generally range between 1.5 and 8 metres. The coals are low to moderate in ash, being mostly below 20% and high in volatiles (25 to 33% air dried). The I.D. temperature of the coal ash is above 1200°C. The coals are low in sulphur (below 0.7%) and phosphorus (below 0.01%). The coal resources of Chirimiri coalfield thus appear to be quite promising.

v) Korba and Bisrampur Coalfields

These two coalfields account for a total reserve of over 130 million tonnes of fair to medium quality non coking coals. The coals are rélatively low in ash (below 18%), sulphur (below 0.6%) and phosphorus (below 0.01%). The I.D. temperature of the coal ash is also high (over 1200°C). Although the coals are slightly lower in volatiles (25 to 28% air dried) as com-

pared to other coals, it is important to note that the productions in both the coalfields come from a single seam i.e. from Pasang seam in Bisrampur coalfield and Ghordewa (G-III) seam in Korba coalfield. Furthermore, the production potentialities of this coalfield are high. The present annual production target of coals are 2.7 million tonnes from Pasang seam (from 3 collieries) of Bisrampur coalfield and a little over 2 million tonnes from Ghordeva seam (3 collieries) of Korba coalfield.

vi) Rampur Coalfield

Rampur coalfield of Orissa working Rampur and Ib seams has a total reserve of about 40 million tonnes of low to medium ash coals. The seams are generally 2 to 3 metres in thickness. The coals from Ib seam is relatively low in ash (below 16%) but is also somewhat low in volatile matter (23 to 25% air dried). The coals from both the seams are low in sulphur (0.2 to 0.5%) and phosphorus (0.005%). However, the I.D. temperature of the coal ash sometime shows a lower trend of 1130°C or so.

vii) Talcher Coalfield

The Bottom seam (2 to 7.5 m) worked in 3 collieries of Talcher coalfield of Orissa has a total proved reserve of about 110 million tonnes. The coals are comparatively low in ash (13 to 18%), high in volatiles (33 to 35% air dried) and low in sulphur (0.4 to 0.7%) and phosphorus (below 0.01%). The I.D. temperature of the coal ash is also fairly high (above 1150° C). The present production target of this seam, from the 3 collieries is over 1.4 million tonnes per year.

viii) Pench Valley Coalfield

Situated in the western part of Madhya Pradesh, the Pench Valley coalfield accounts for a total reserve of about 190 million tonnes of fair to medium quality (ash 14 to 24%) coals, produced from 3 to 4 working coal horizons. The coals are fairly high in volatiles (27 to 33% air dried) with I.D. temperature of the coal ash always above 1200°C. The sulphur content of the coals at times higher (unto 1.9%).

ix) Umer and Kamptee Coalfield

Situated in the state of Maharashtra, these two areas near Nagpur account for a total reserve of about 120 million tonnes of medium quality (ash 14 to 21%) coals worked in two collieries viz. Umrer and Silewara (Kamptee) mines. The coalash generally shows somewhat lower range of fusion temperature, although the I.D. temperature is always over 1100°C.

x) Wardha Valley Coalfields

The 7 working collieries of Wardha coalfield, working different sections of a thick composite seam, account for a total reserve of over 140 million tonnes of coal. Although the coals contain ash below 20%, the sulphur content of the coals is generally on the higher side (0.8 to 1.8%). The coal ash shows somewhat lower range of fusion temperature, although the ID temperature is always above 1150°C.

xi) Godavari Valley Coalfields

Situated in Andhra Pradesh, the Kothagudium Tandur and Ramagundam areas of Godavari Valley coalfields are the other potential regions having coals suitable for sponge iron industry.

Of these, Kothagudium area, working Queen and King seams, with a reserve of about 220 million tonnes appears to be important. The ash in the coals lies between 15 and 24% with sulphur mostly below 1% and phosphorus below (0.01%). The I.D. temperature of the coal ash is high (above 1340°C).

The other two areas working Seam No. 1 to IV have a total reserve of over 578 million tonnes. Although the coals of these two areas are also similar in quality the sulphur content of Ross Seam (i.e. Seam II) in Tandur area is generally high (upto 2%). In Ramagundam area, the I.D. temperature of coal ash sometimes shows the tendency to be on the lower side (below 1100°C).

xii) Neyveli (South Arcot) Lignite Field

Situated further south in Tamil Nadu, the Lignite deposit of Neyveli has a proved mineabble reserve of over 600 million tonnes which also appears to be attractive. The lignites at a moisture level of 15 to 20% (air dried) has ash of 4 to 6%. They are low in sulphur (generally below 1%) and phosphorus (below 0.01%). The I.D. temperature of the coal ash is relatively high $(1180^{\circ}-1220^{\circ}C)$, although the ash fusion range is somewhat low $(1180^{\circ}-1380^{\circ}C)$.

Availability of low ash coals

It is apparent from Table II that the ash limits of coals suitable for sponge iron manufacture have been considered generally upto 24%. However, if it is desired that the ash in the raw coals should be low, say, upto 16% or so, the potentialities of the areas containing such coals, along with their properties, are given in Table III.

Thus, relatively low ash coals are available

from Sohagpur (Jhagrakhand and Kotma areas), Bisrampur. Chirimiri and Pench Valley coalfields of Madhya Pradesh, Talcher and Rampur coalfields of Orissa and Ranigani coalfield of West Bengal. These coals are mostly low in sulphur (below 0.7%) and phosphorus (below 0.01%). The phosphorus contents of Ranigani coals are comparatively high (around 0.1%). The I.D. temperature of the coal ash is also generally high (above 1150°C), except those of Raniganj, Kotma and Rampur coals where it is generally 1100° and 1200 °C. The total rebetween serves of such low ash coals (ash below 16%) would be well over 1200 million tonnes. Of these, Bisrampur, Talcher, and Jhagrakhand areas appear to be attractive.

Use of medium ash coals after beneficiation

Studies on the available data on cleaning characteristics of coals of medium ash group (ash 17 to 25%) indicate that these are amenable to washing with reasonably good yield of cleans.

A broad generalisation of the cleaning possibilities such medium ash coals are given in Table IV:

Table IV Cleaning possibilities of medium ash coals.

n:	4.1.0/	Sp. Gr.	Cl	eans	Si	nks
Particulars	Asn%	cut around	Wt%	Ash%	W1%	Ash%
Överall	17	1.50	60	13	20	30
raw coal	to		to	to	to	to
	25		×0	15	40	45

It is possible to have 60-80% yield of cleans with ash 15% or below at a specific gravity of separation around 1.50. The corresponding sinks with 30-45% ash may be considered suitable for pulverised fuel firing in large boilers. At times when the coals contain distinct shale bands the ash of the sinks may be still higher (50-55%) with consequent increased recovery of cleans. The clean coals can thus be used after dewatering to a reasonable moisture content.

Use of low temperature char as solid reductant

As indicated earlier, use of formed coke10 produced from chars of non coking coals as alternate fuel for blast furnaces can be effective means of conserving coking coals whose availability is limited. In an integrated scheme, formed coke may be used as substitute of coke in the conventional blast furnace and sufficient 'char' may be manufactured for use as solid reductant in sponge iron plant. The 'char' from a typical Indian nen coking coal by fluid bed carbonisation at 500-550°C has the properties given in Table V below:

Table V

Properties	of	L.T.	char	from	a	typical	non	coking
			Indi	an co	al			

M	3-5%	Real density:	1.6-1.8 g/c.e.
Α	20.24%	Bulk density:	$365-415 \text{ kg/m}^3$
VM	10-12%	Reactivity to C	CO ₂ —180-185.

The char being a reactive solid, may be suitable for the purpose of reduction of iron ores, where the heat required for the process can be supplied by firing pulverised coal of the type from which char is produced.

Conclusion

In view of the attempts that are being made to by-pass the conventional blast furnace route of steel making and the increasing importance of the direct reduction technique for the production of sponge iron, it is thought worthwhile to assess the quality and quantity of solid reductants available in India suitable for the purpose. It is felt that the coals from Talcher, Bisrampur and Jhagrakhand coalfield may be eminently suitable for the process because of their superior quality. The coals from Kothagudium area of Godavari Valley coalfield and the lignites from Neyveli also deserve attention because of their geographical positions. Char obtained from integrated 'formed coke' plant produced by carbonising non coking coals in fluid bed at low temperature may also be utilised with advantage.

Acknowledgement

The opinion expressed in this paper is of ¹⁵. the authors' and not necessarily of the Central Fuel Research Institute. 16

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Reference

- 1. Lahiri A. FRI News, 18, 4 (1968), 118.
- Ghosh P.C. and Lahiri, A., (Reprint) J. 19. Min, Met. Fuel 18, 11 & 12 (1970) 1.
- Miller J.R., 'The production and use of directly reduced iron ore' Paper presented 20. at the Silver Jubilee Symposium, Indian Instt. of Metals, New Delhi, Feb. (1972).

- Altekar, V.A., Chatterjee A.B., Gupta K.N., Mathur G.P., and Kapoor A.N., 'Some experiences on direct reduction with non coking coals in a rotary kiln, (Ibid).
- 5. Janke W., The SL/RN process—Development and Experience (Ibid).
- 6. Ray P. Litton and Gunther H. Miller 'Development and Growth of the HYL process, (Ibid).
- 7. König H., Problems of prereduction of iron ores and their economic aspects (Ibid).
- 8. Baneriee N.G., Sarkar G.G., and Lahiri, A., India in Industries, 2 (1957) 36.
- 9. Banerjee N.G., Moitra A.K., Paper presented at the symposium on Coal Mining Industry at CFRI, Jan. (1970).
- Raja K., Moitra A.K., and Lahiri A., Alternate fuels for blast furnaces Paper presented at the Silver Jubilee Symposium, Indian Instt. of Metals, New Delhi, Feb. (1972).
- Report of task force on Coal and lignite, April (1972), Planning Commission, Govt. of India.
- Report of the Committee on Assessment of Resources, volume II, Ranigani coalfield (1963).
- 13. Report on the utilisation of South Arcot lignite, CFRI (1954).
- 14. Raychaudhuri K.K. & Deshmukh, B.S. Chirimiri Coals', CFRI (1964).
 - Raniganj Coal Survey Laboratory, Annual Reports (1957 to 1970).
- Ranchi Coal Survey Laboratory Annual Reports (1965, 1968 and 1969).
- Bilaspur Coal Survey Laboratory, Annual Reports (1956, 1957, 1962 to 1971) and Technical Reports Nos B/2/65, B/3/65, 27, 38 to 42, 47, 48, 50, 55 and 56).
- Nagpur Coal Survey Laboratory, Annual reports (1957 to 1971) and Technical report Nos N/1, 2 & 3/65, N/4/65, N 7, 8 & 9165 N/65 N/1/1/67).
 - Nagpur Coal Survey Laboratory, Report on the Rapid survey of Kothagudium Yellandu and Tandur Coalfields, (1953-1957)

Report of the washability studies of Non coking coals from Wardha Valley, Kamptee and Godavari Valley coalfields, CFRI (1961).

Discussion

Mr. A. N. Naik (Tata Iron & Steel Co. Ltd., Jamshedpur). i) What is the crushing strength of formed coke and its cost of production as compared to the conventional blast furnace coke that is now produced in integrated iron and steel plants, ii) How long will it take to instal new coke ovens for the production of formed coke if it is more economical than B.F. coke as none is at present existing?

Mr. K. K. Raychaudhuri (Author) (i) The crushing strength of formed coke is not fixed. It depends on the type of formed coke and its use, i.e. whether for domestic, industrial or metallurgical purposes. For example the point crushing strength of formed coke prepared from non-coking Indian coals has been found to be 275 kg, which is suitable for metallurgical purpose.

The cost of production is also dependent on the process or scheme followed for the preparation of formed coke and the capacity of the plant. However, the cost of production of formed coke by adopting a particular process may be comparable to that of the commercial coke price as at present. (ii) A commercial formed coke plant can be set up at least 3 years after final decision is taken for installing such plant and necessary action is initiated.

Mr. T.V.S. Ratnam (M.N. Dastur & Co. P. Ltd., Calcutta). You have mentioned about large blast furnaces and the quality of the new materials required. Will the coke produced from the Indian coals have adequate strength for use in large blast furnaces? What are your views in regard to the strength of the coke for large blast furnaces?

Mr. T.V. S. Ratnam (M.N. Dastur & Co. P. Ltd., Calcutta). Coke produced from 100% washed Jharia coals (Prime caking) conform to the stringent international specification of Physical characteristics of coke required for large blast furnaces. Although we do not have much experience of using cokes produced from Indian coals for large blast furnaces, cokes produced from blend of 50% prime coking coals (Jharia) and 50% medium coking coals (Kargali) both washed, are successfully being used in 2000 cu.m. blast furnace of Bokaro Steel. The Russian specification for cokes to be used in such furnace is Micum, M_{40} -79 to 80 and M_{10} -10 of less. How these cokes would behave in blast furnaces of larger capacity cannot be envisaged at the moment.

Table I. SOME DIRECT REDUCTION PROCESSES WHERE SOLID REDUCTANTS ARE USED

PRO CESS	IN OPERATION AT	REDUCTANT		AVERAGE AN	ALTSIS OF 1	UEL	
			¥.	- R	X.M.Y	F.C.\$	2
1. Krupp-Renn	EAST AND WEST GERMANY POLAND, CZECHOSLOVAKIA, NORTH KOREA. GREEGE	Coke	•	•		55.0	
	JAPAN, SPAIN AND U.S.S.R.						
2. SL-RN	U.S.A, CANADA, BRAZIL, DEEDT SOUTH ARDICA	Lignite	31.5	0-7-0-4	30.0-	31.0- 50.0	0.5
	AUSTRALIA, NEW ZEALAND,	Coal		8.0	36.0	55.0	•
	JAPAN, SOUTH KOREA	Anthracite	•		10.0-	-0°89 70°0	0.6-0.7
	(NML) FIDIA	Coal (Maharashtra)	9.5	16.5	31.2	42.8	I
		(~La (A.P.) Lao	6.0	28.3	21.6	2+17	1

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QUALITY PROPERTIES AND POTENTIALITIES OF COALS

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	eserves	noilim	191	-2317	2		707 -		820		411	ţ,	5			9		78		436		98		65		10.2	ļ	C 01 41		
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-90% E	Ash	28	141	12	3 2	14	\$	28	<u>۲</u>	52	ñ	\$ 2	5	36	:	F 9 8		¥8₽	1	38		t 1	21	54	88	ង ដ	32	14	24	
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Seams 1 1				All working	seams (of Rani- ganj series)	*#11 workfoo	8888.		Upper coal	norizons upto Argada A (working)	Bottom		Rampur	4 L		Ghordswa (G-III)		Pas ang	All		, contraction of the second seco	A 45 B		Irea All working	s pana.	area Dhanpuri		ry "Alt working	sears.	
Coalfield -				Raniganj	k Eastern & Eastern Sactor)		Karanpura		South	karanpura.	Talcher		Rampur			Korba		starenpur	Chirimiri		Sohagpur 1.1 Thomas	BEBG		11) Kotma A		111) Burhar		Pench Valle		

1			। व 	10				11		-11-11-	12	11111	_ 14	15.1.5	
Kamptee (Sileware	NI	a \$ 6	363	36'38	39 410	5110 to 5175	* 9:-	0.005 to 0.01	41 420	8 0 0 8 0 0	4.5 4.0 5.0	×	I.D-1110-1345 H.P 1245-1400	ស្ត	
Umrer	Top,Middle and Bottom	4 9 4	20 ¢ 1	363	45 to 2	5000 to 5400	to 5 1,0	0.02 40 0.03	35 39 39	77 to 01	4.3 4.7	×	I.D 1170-1240 H.P 1260-1380	85	
Wardhe valley (7collierie	All working sections) of a thick- seam.	5 ti a	5 t 12	888	45 to 39	5280 to 5720	1.8 1.8	0.1 0.1	4 to 19	40 81 81	4.8 5.3	¥	I.D1150-1295 H.P 1285-1390	141	
Codeveri ve. 1)Remagumder area (South Eoc vari)	Lley a 6 All working ic te-8 Seems.	9 2 0	53 55	36 23	434	6250 to 6890	to 4	0.001 to 0.009	4 te 3	ឌ ជុំ ឆ្ល	to 5.4	*	I.O 1080-1380 H.P 1270-0ver 14	900 378	• S% moatly low.
11)Kothegudi area.	um All working seam.	r \$ a	5 th 15	885	40 50 40 50	5310 to 6100	te 0	upto 0.006	P 3 4	83 0 23 83 0 23	5 to 5	×	I.D., 1340-1400 H.P ovar 1400	219	e S% mostly love
111) Tendur eree	All working seams	844	54 to 24	33 6 33	434	5200 to 5800	. 1:9 1:9	0.001 to 0.005	4 to 4	83 to 8 0.	4.6 5.4	-		200	• 5% in Ross seam mostly high
Neyvlis	Lignites	82 ¥	044	433	1 12 2 2	4725 4725 to 6300	- 22 - 22 	0.001 to 0.006	53 1 53 1 53 1	0°02	1 0 °S	 <	I.D. 1180-1220 H.P. 1340-1380	over 600	

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	Remarks	*Proved class II quality		برخ Risserva figure مرخ available.		سند ۲۰	"Indicated reserve		Separate reseve figure rot avai labie.
	C Total		-1280 46 - over 1400	-1180	-ovar 1400 r 1400 78	r-14600 97	-1240 *71 1400	- 1280 1400 39	-over 1400 1400 -
	Ash Fusion temperature (under midiy reducing atm	1.0.1 1.0.1 1.0.1 1.0.1 1.0.1 1.0.1 1.0.1	H.P1390	I.D1120 H.P0VBI	I.D1210 H.P 0V8	H.P.C. 117	I.D. 1160 H.P. over	I.D. 1120 H.P. over	I.D. 1200 H.P. over
	LTC coke type		8	۲.	<	2 2 2	4	œ	© 3 ≪
ASH COALS	Un demire basis V. M. S.	រ ខ្លួំង ខ្លាំង ខ្លាំង ខ្លាំង	42 46 66	ន	35 to 3	ន្លន្ឋ	4 0 Q	ម្លូង ទី	8 t t 2 t t 2 t
ITIES OF LOW	Phosphorus	1	to 0.007	0.003 to 0.004	balow 0,004	0.002 to 0.004	balow 0,004	0,003 to 0,004	0.005 to 0.05
POTENTIAL	Sulphur	0.3 to 0.6	0.6 to 0.7	0.3 to 0.6	below 0.6	0.4 0.7 0.7	balow 0.5	0.4 to 0.7	0.0 1.5
ROPERTIES AND	basis Calorific value (K.cal/kg)	5700 to 6300	6100 to 6650	6050 to 6400	5650 to 5800	6200 to 6750	6100 to 6550	5800 to 6250	6100 to 6500
UALITY, P	- at 40°C	1 1 1 2 2 8 1 1 1 1 1 1 1 1 1 1 1 1 1 1	44 46 46	54 54 54	49 52	50 58 58	55 55	53 t 48	44 49
	H. W. W.	535	638	22 5 33 24 5 33	25 28 28	32 23 23	858	ះ រ រ	5 9 F
	10 Lask	1 5 8 5	235	234	12 G 12	252	1 12 12 12	255	5 3 5
	Moist	1 ~ 2 P	8 to 7	۳3°	°35	ちせて	2°2 2°2	က ဦတ်	а С С
		Upper Kajora. Jambad- Bankola, Samla.	Main (Bottom)	Ib	Pas ang	No.3 (Karakoh, Main of Goffela) No.3A (No.4) Sonwani.	۰۷.	Kotma Top, Kotma Sottom, Silhara	Pench sear (Sean 1) Pench Botto m Seam 1) (Seam 1) Searn 1
	Collieries	Collieries in eastern sector.	Talcher, Deulbera, Handidua	Örient	Kumda Inclines, Paseng Joynagar Quarry and Inclines,	West Chimiri New Chimimiri Chimiri Kurasia, Uuman Hill Sonwani,	Rajnagar and Ramnagar,	Kotma	Jatachhapar Ek éah d ra Raumwara Ranwara, khas, Ambora,
	Coalfield -	Raniganj	Talcher	Rampur	81srampur	Chirimiri	Sohagpur 1) Jhagtiskhand area	íi) Kotma Area	Pench valley